Figure 1a - UV Absorption of Combustion Gases

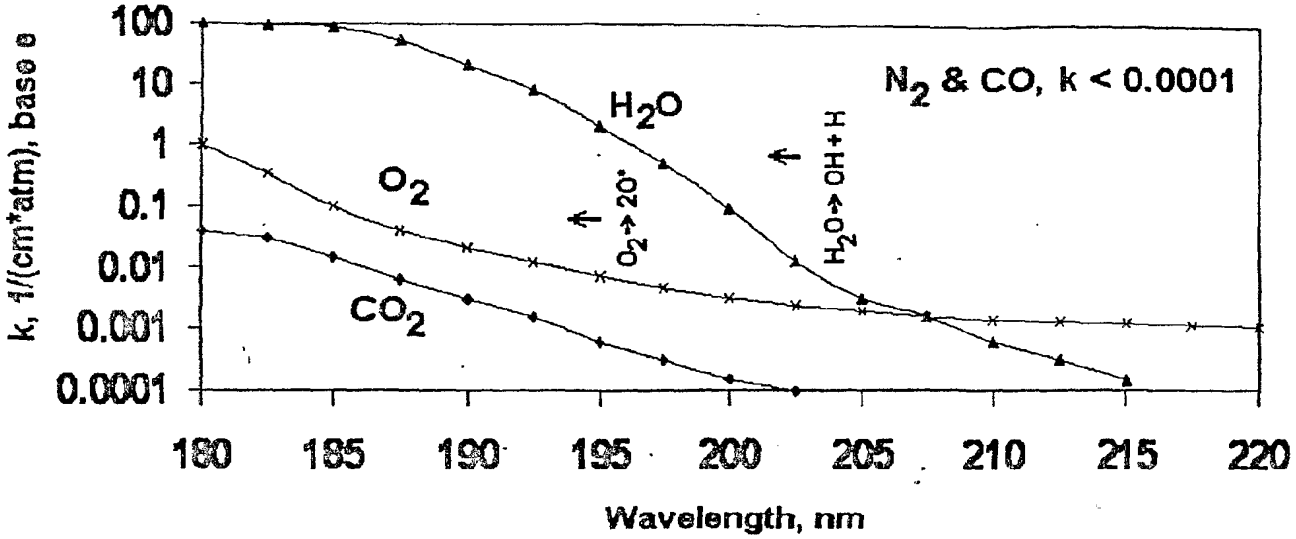


Figure 1b - UV Absorption of Nitrogen Based Gases

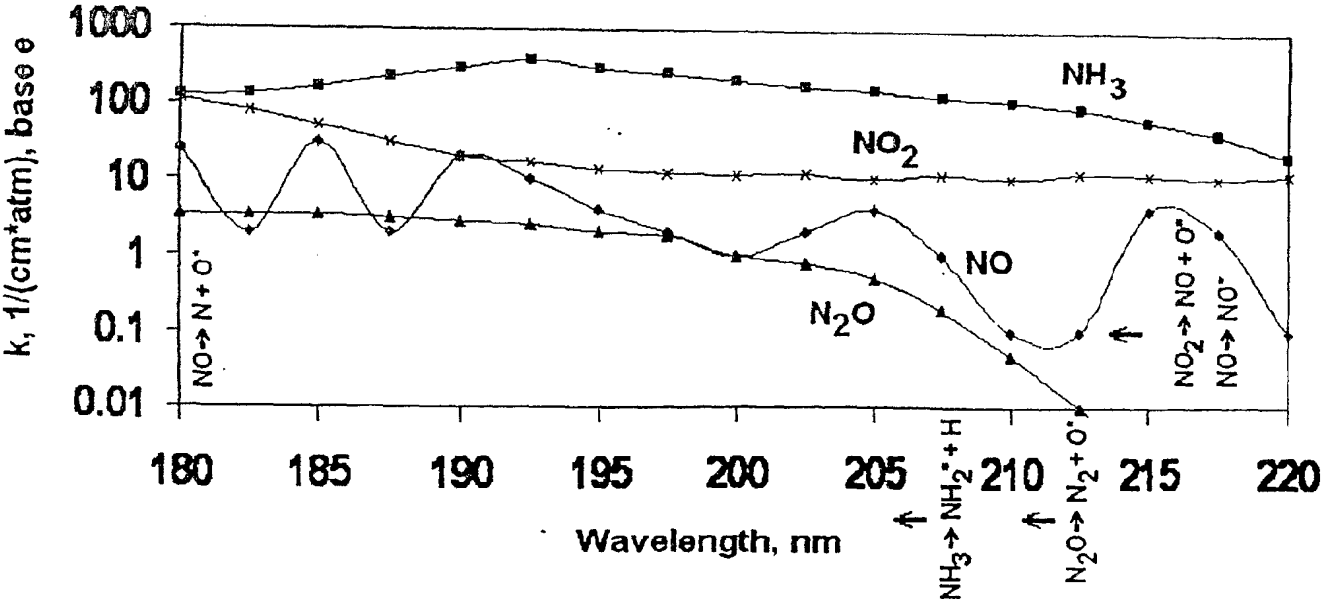


Figure 1c - Important Secondary Reactions

Oxidation

$O' + CO \Rightarrow CO2$
$O' + NO \Rightarrow NO2$
$O' + H2O \Rightarrow 2OH$
$O' + NH3 \Rightarrow NH2' + OH$
$OH + CO \Rightarrow CO2 + H$
$OH + CH2O \Rightarrow H2O + HCO$
$OH + NO \Rightarrow H + NO2$
$OH + NO2 \Rightarrow HNO3$
$OH + NH3 \Rightarrow NH2' + H2O$
$HCO + O2 \Rightarrow HO2 + CO$
$H + O2 \Rightarrow HO2$
$HO2 + NO \Rightarrow OH + NO2$
$HO2 + CO \Rightarrow OH + CO2$

Reduction

$NH2' + NO \Rightarrow N2 + H2O$
$NH2' + NO2 \Rightarrow N2 + H2O2$
$H + N2O \Rightarrow N2 + OH$
$H + NO \Rightarrow HNO$
$H + NO2 \Rightarrow HNO2$
$H + O2 \Rightarrow HO2$
$H + CO \Rightarrow HCO$

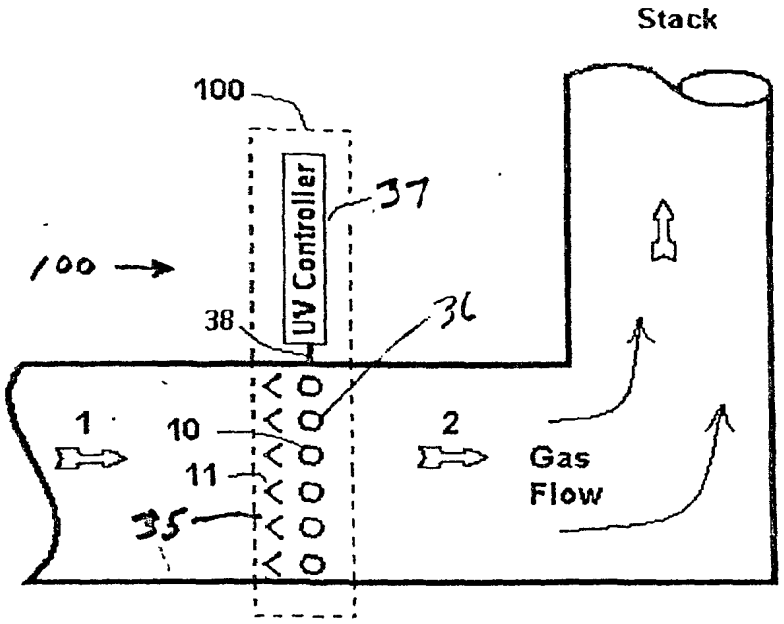


Figure 2a - Use of SUVR to Destroy Combustion Contaminants and/or VOC's

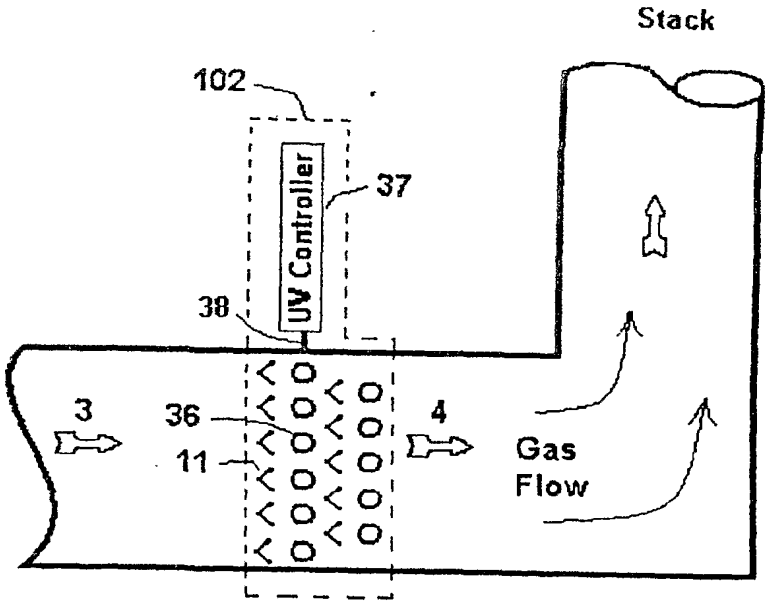


Figure 2b - Use of SUVR to Polish Residual NO_X and NH_3 Gases from an Upstream SNCR, SHR, or SCR Process

Figure 3a - SUVR to Control Combustion Contaminants and/or VOC's plus NO_X Emissions

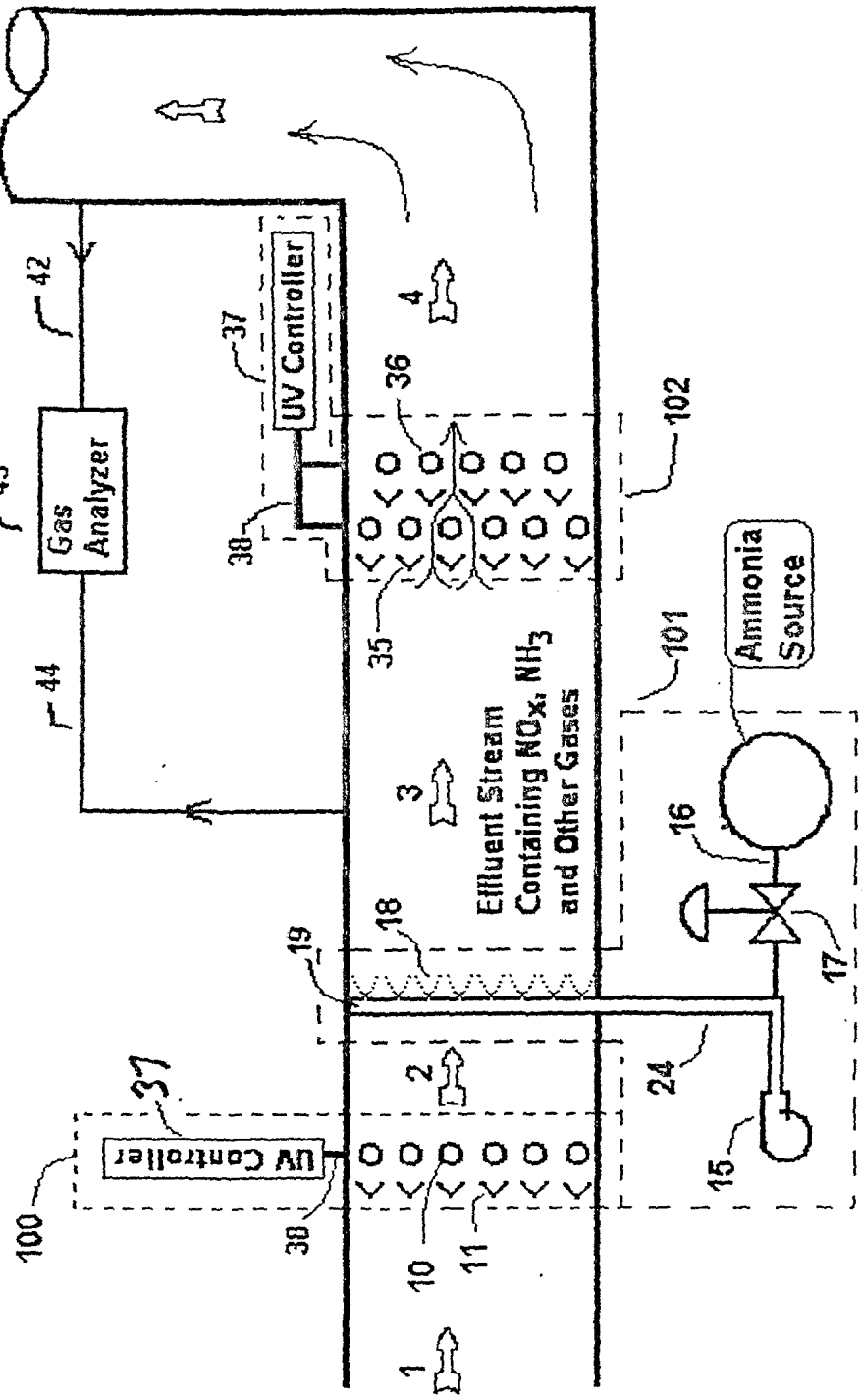
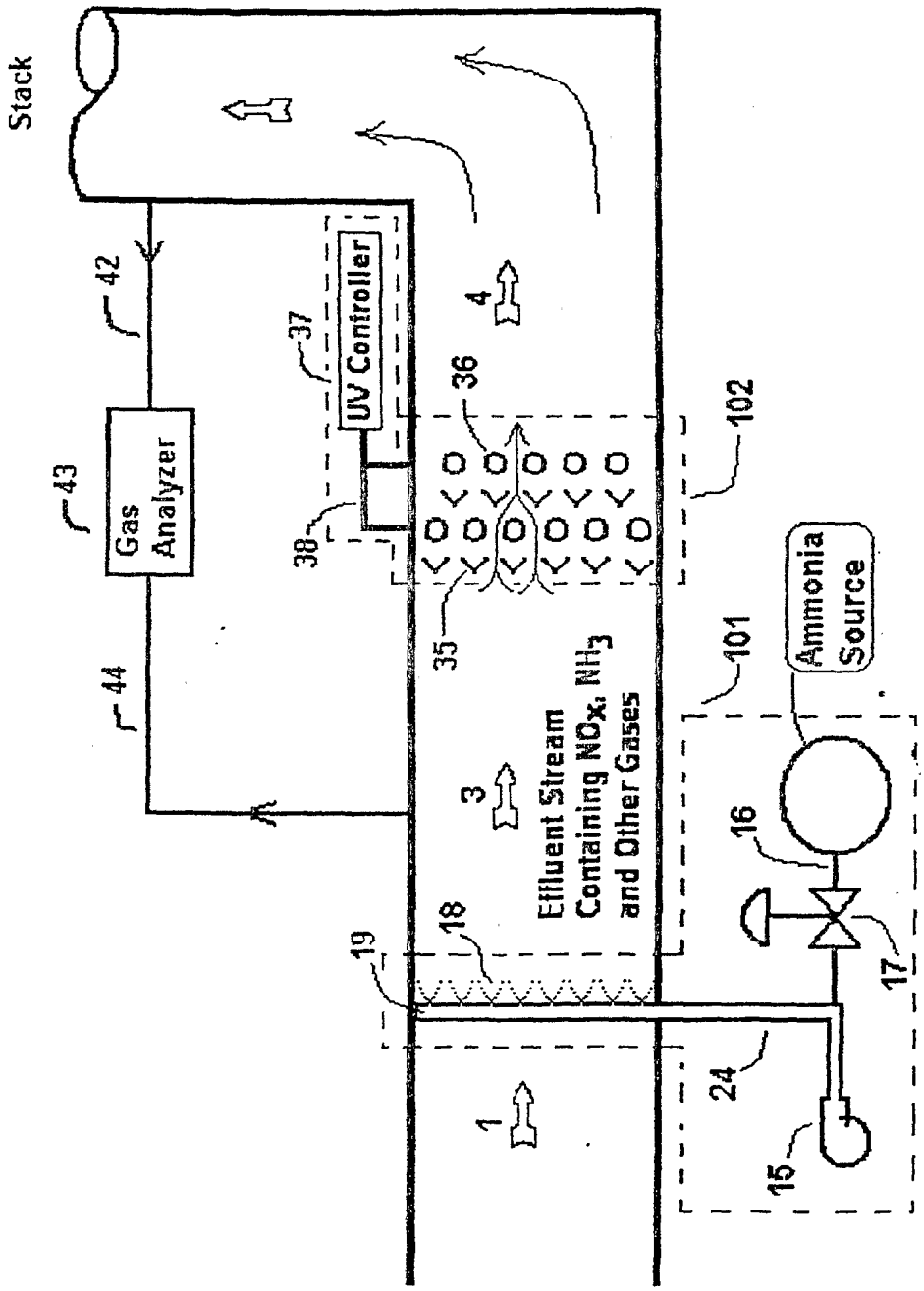


Figure 3b - SUVR to Control NO_x Emissions



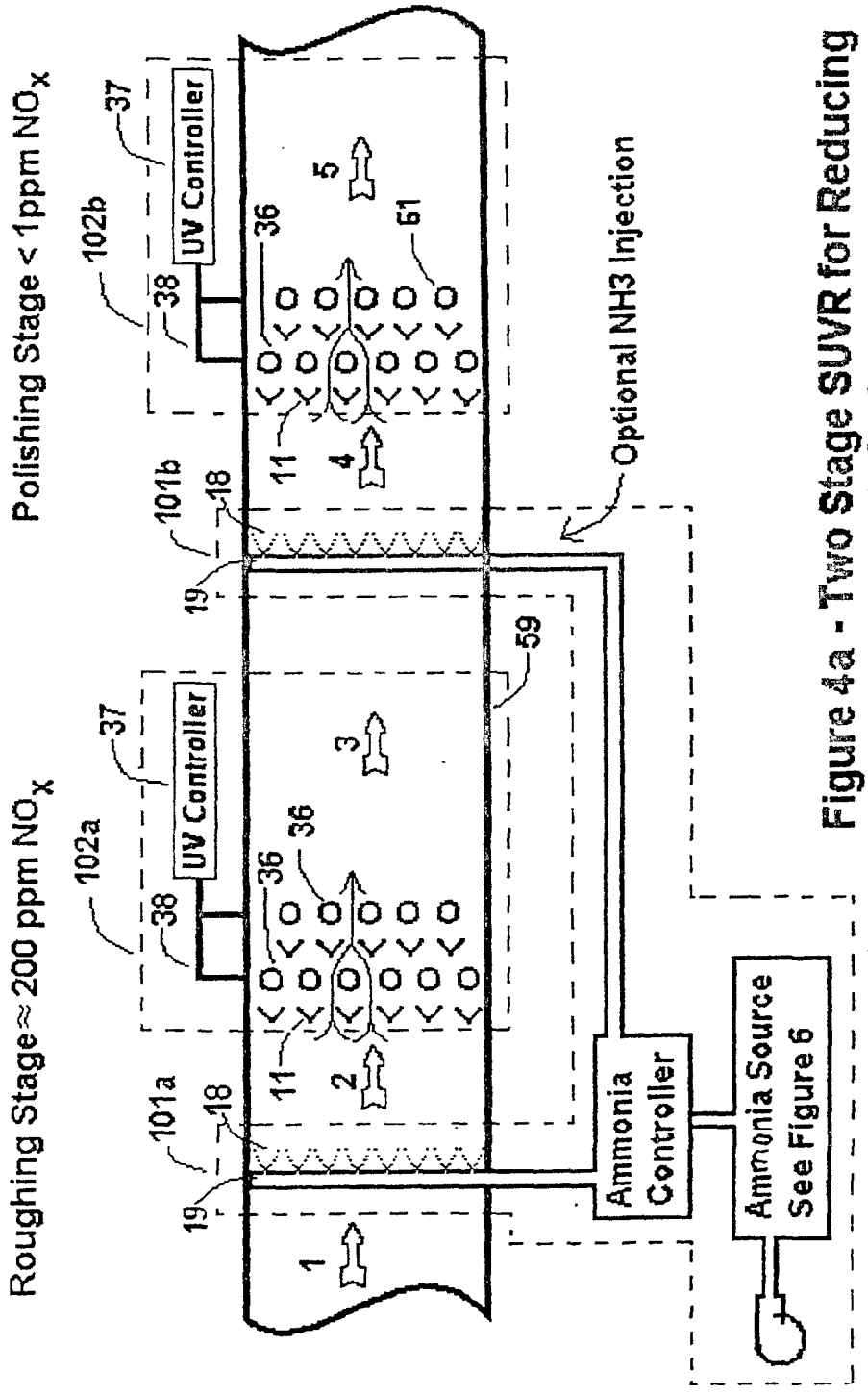


Figure 4a - Two Stage SUVR for Reducing NO_x Emissions

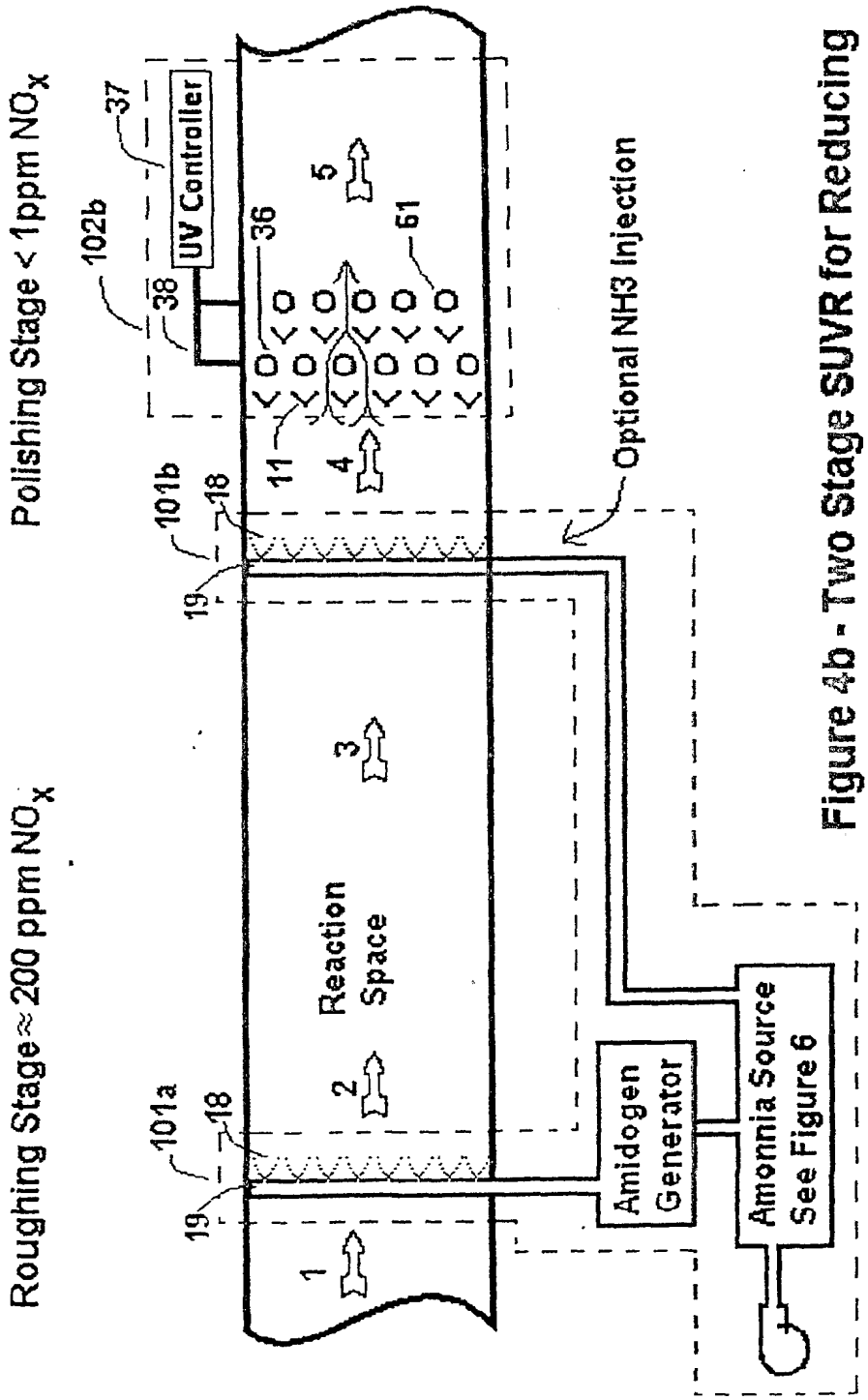


Figure 4b - Two Stage SUVR for Reducing NO_x Emissions

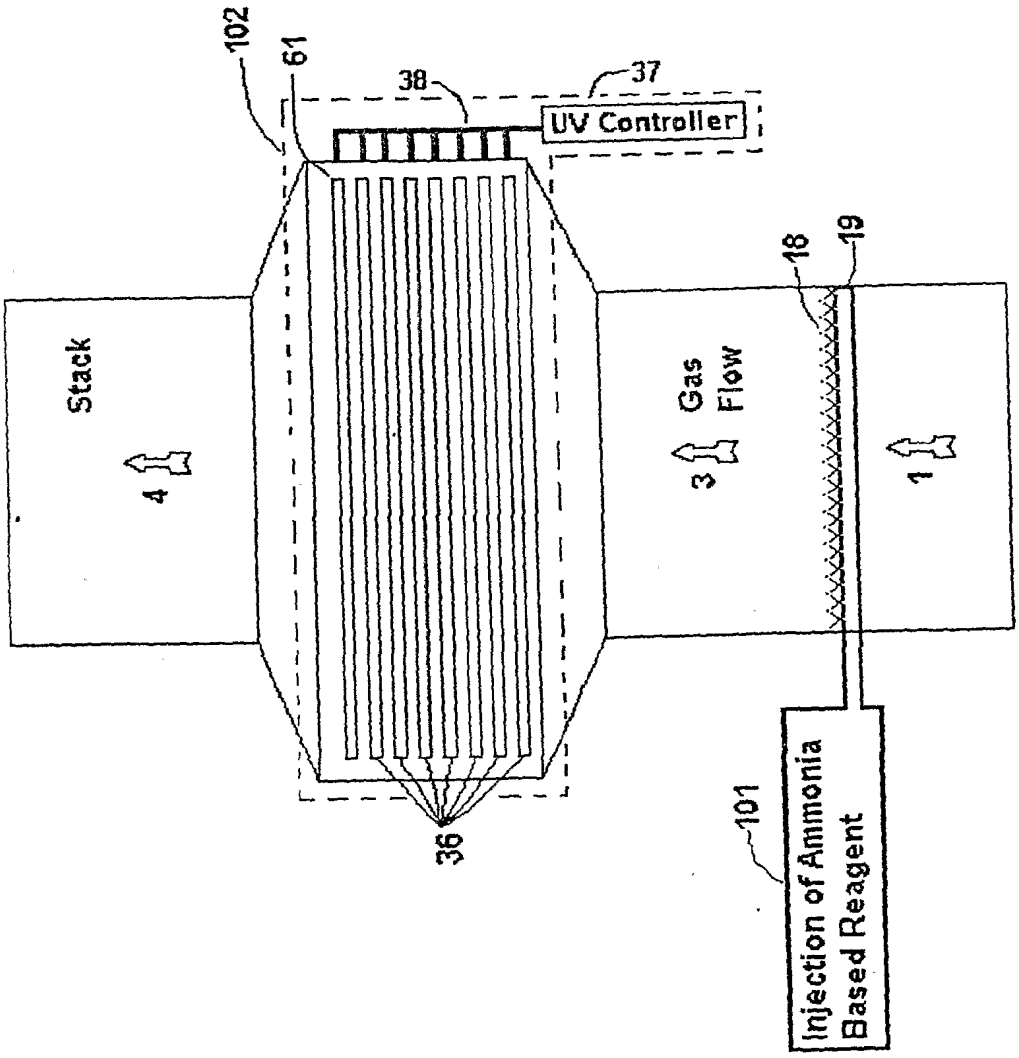


Figure 5 - Installation of the SUVR process on a Combustion Device to Remove NO_x and Residual NH_3 Emissions; Replacing the SCR Process

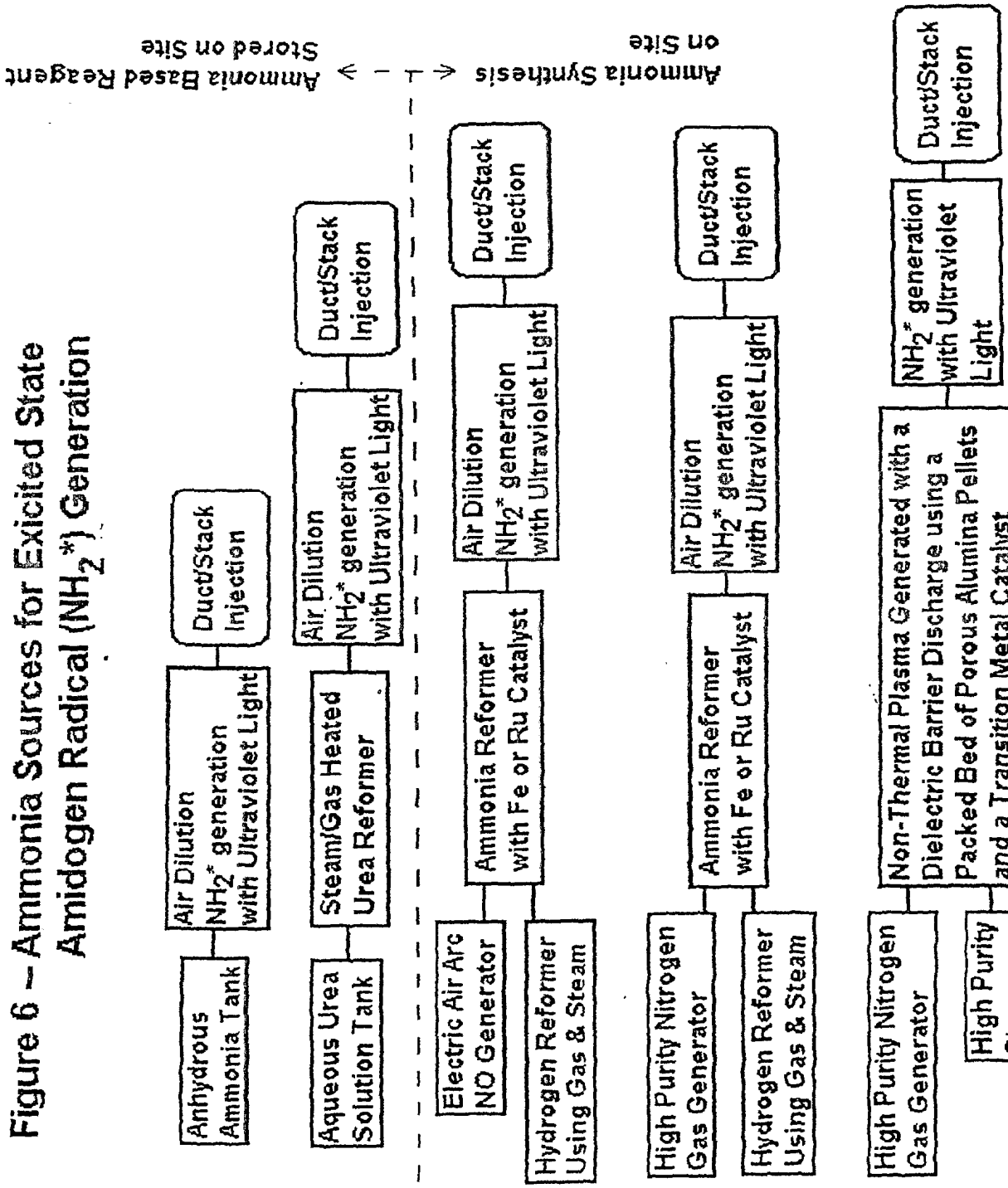


Figure 6 – Ammonia Sources for Exicited State Amidogen Radical (NH_2*) Generation
Ammonia Synthesis on Site
Ammonia Based Reagent Stored on Site
Anhydrous Ammonia Tank
Air Dilution NH_2* generation with Ultraviolet Light
Duct/Stack Injection
Aqueous Urea Solution Tank
Steam/Gas Heated Urea Reformer
Air Dilution NH_2* generation with Ultraviolet Light
Duct/Stack Injection
Electric Air Arc NO Generator
Ammonia Reformer with Fe or Ru Catalyst
Air Dilution NH_2* generation with Ultraviolet Light
Duct/Stack Injection
Hydrogen Reformer Using Gas & Steam
High Purity Nitrogen Gas Generator
Ammonia Reformer with Fe or Ru Catalyst
Air Dilution NH_2* generation with Ultraviolet Light
Duct/Stack Injection
Hydrogen Reformer Using Gas & Steam
High Purity Nitrogen Gas Generator
Non-Thermal Plasma Generated with a Dielectric Barrier Discharge using a Packed Bed of Porous Alumina Pellets and a Transition Metal Catalyst
NH_2* generation with Ultraviolet Light
Duct/Stack Injection
High Purity Steam

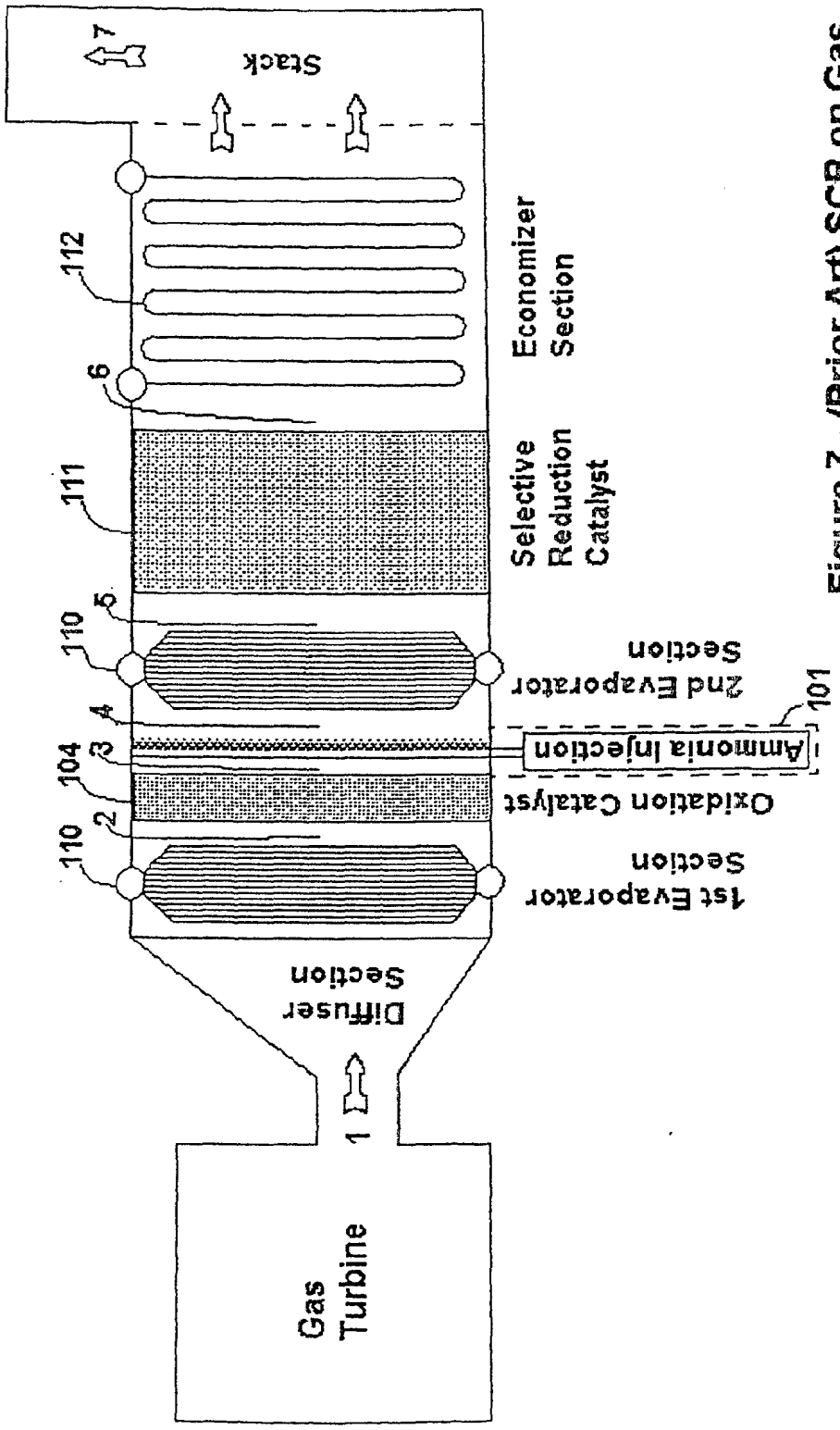


Figure 7 - (Prior Art) SCR on Gas Turbine Waste Heat Recovery Boiler

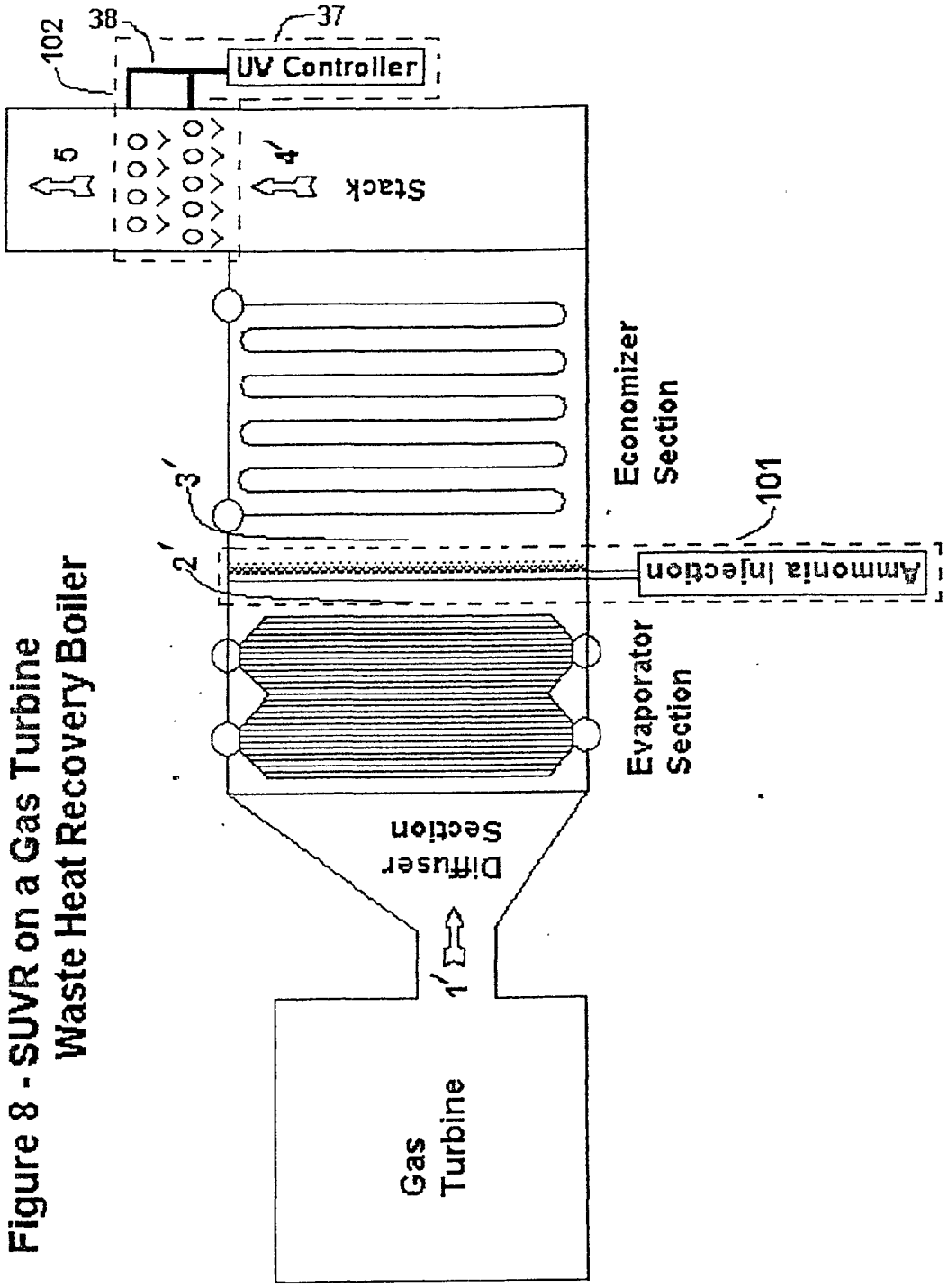


Figure 8 - SUVR on a Gas Turbine Waste Heat Recovery Boiler

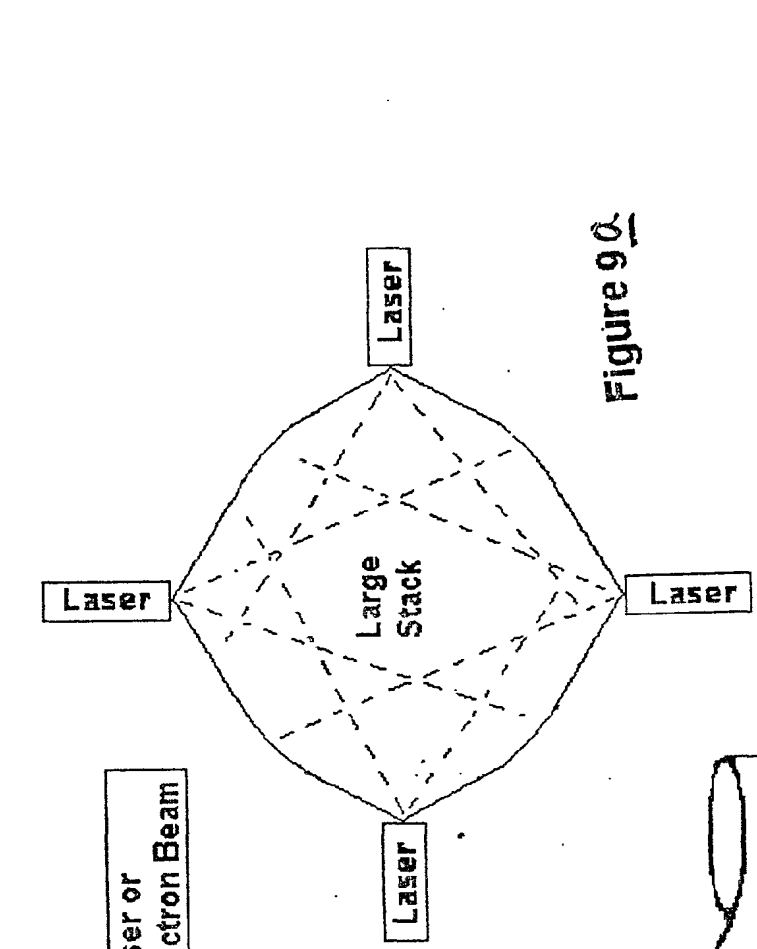


Figure 9a

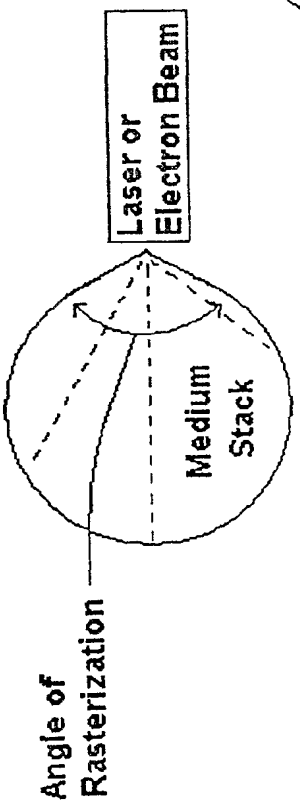


Figure 9b

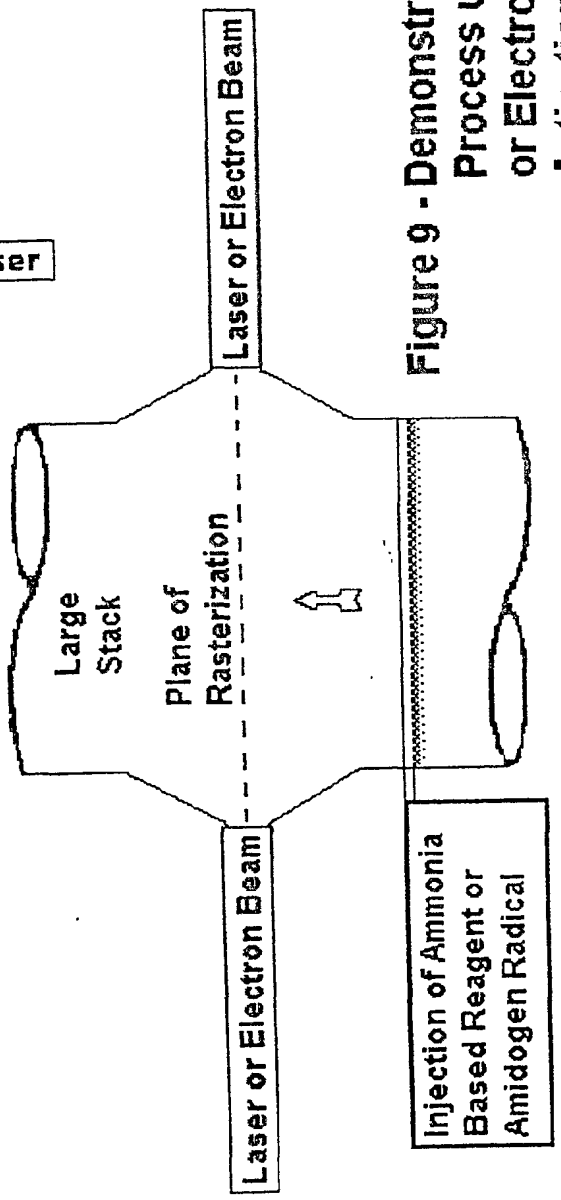


Figure 9 - Demonstration of the SUVR Process using a UV Laser or Electron Beam for Activation

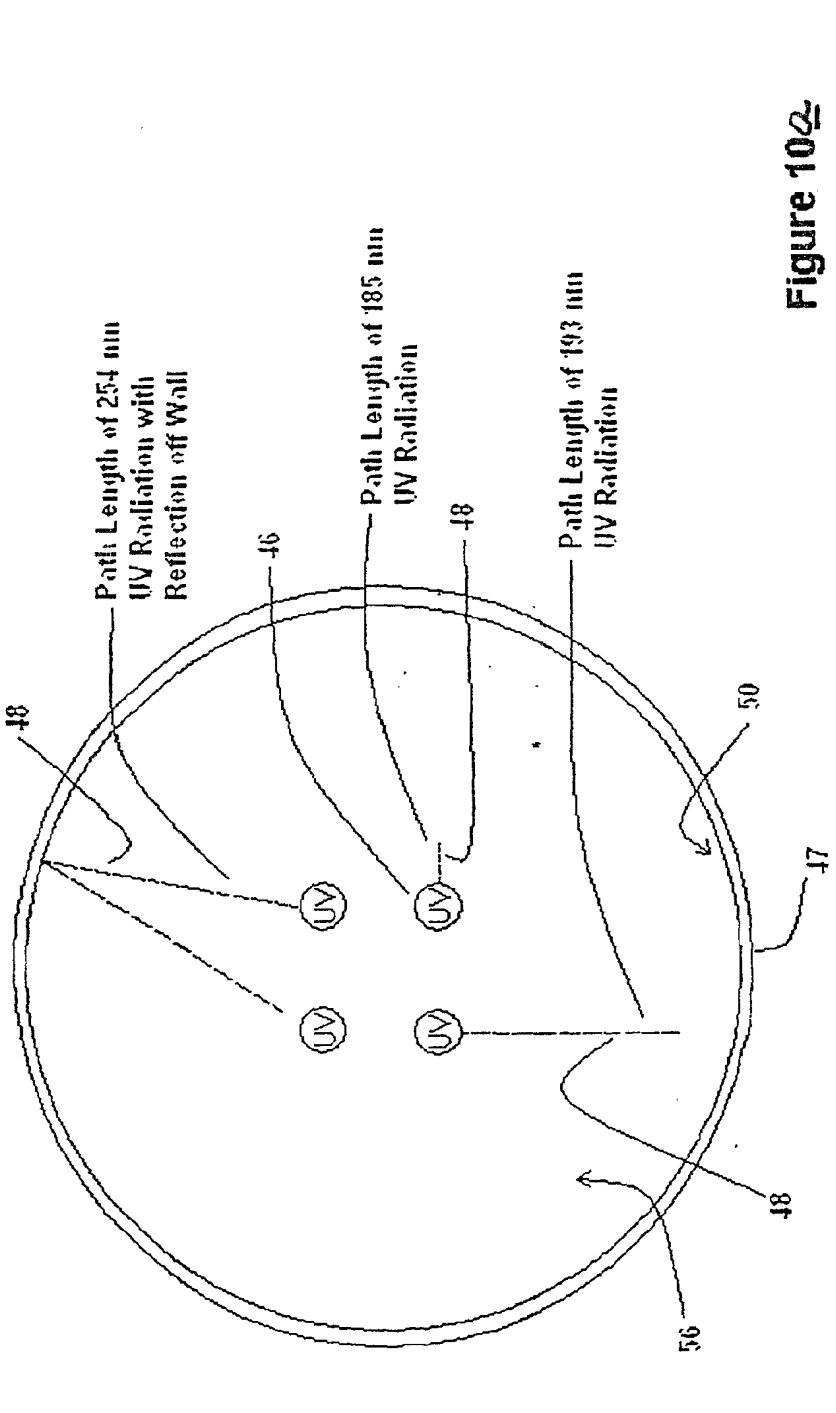
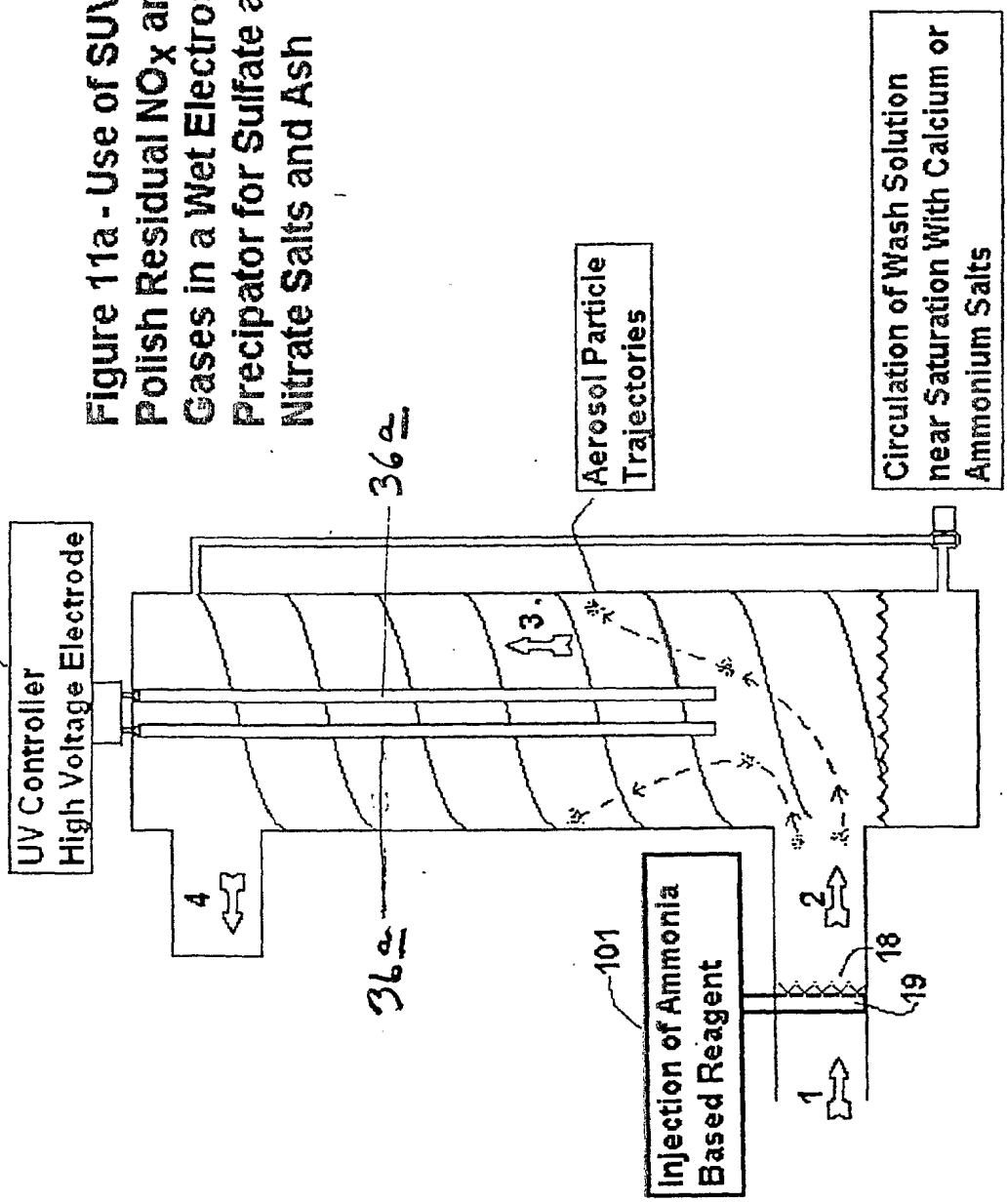


Figure 10 - Relative Transmission Path Lengths of UV lines from a low Pressure Mercury Vapor Lamp

Figure 10a

Figure 11a - Use of SUVR to Polish Residual NO_x and NH_3 Gases in a Wet Electrostatic Precipator for Sulfate and Nitrate Salts and Ash



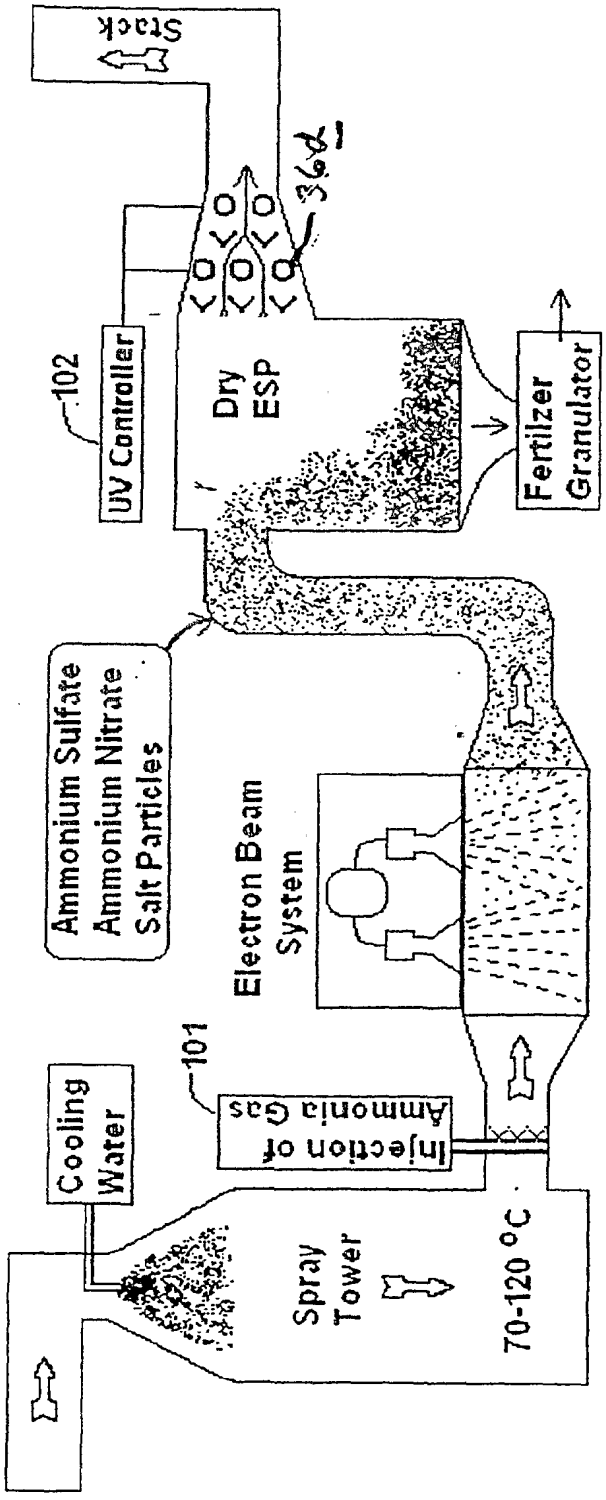


Figure 11b - Use of SUVR to Polish Residual SO_3, NO_X and NH_3 Gases from an Upstream Electron Beam System to Boost Efficiency to over 99%

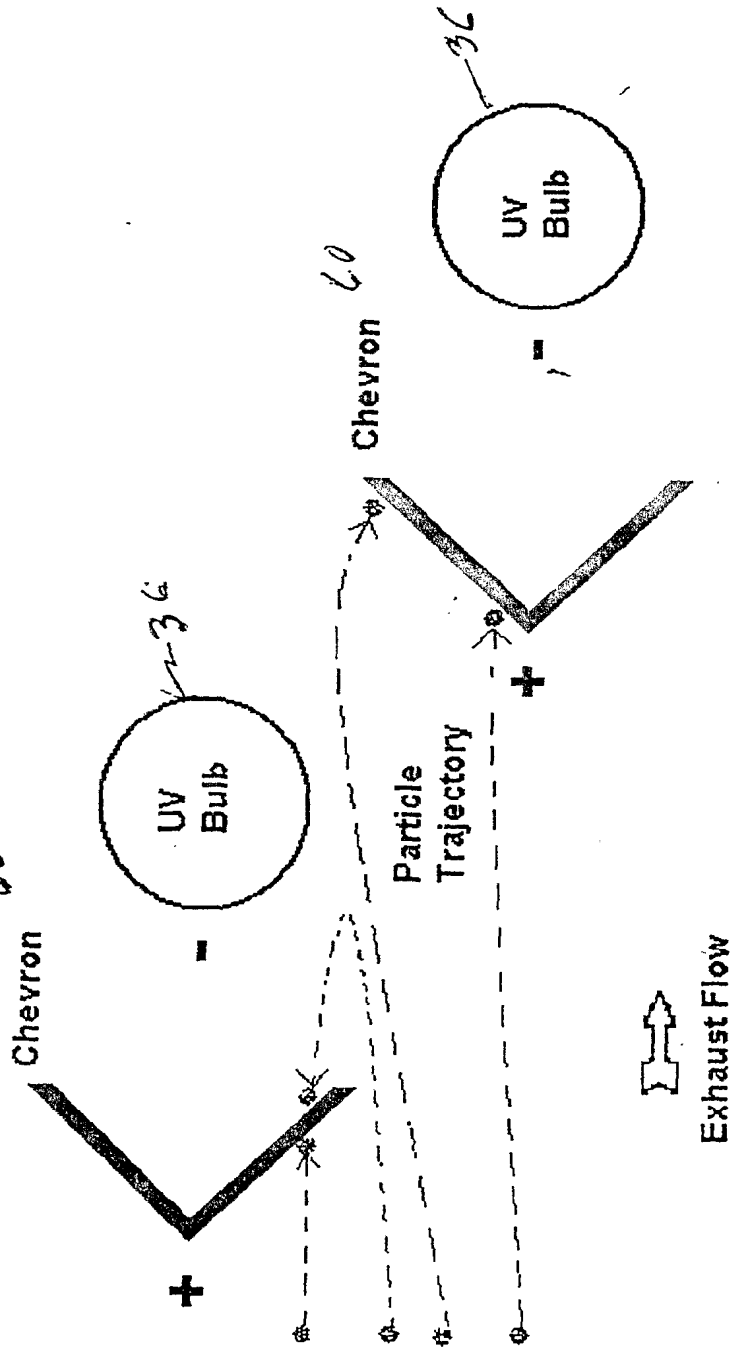


Figure 12 - Electrostatic Field Protection of Ultraviolet Bulbs in Dirty Exhaust Gases

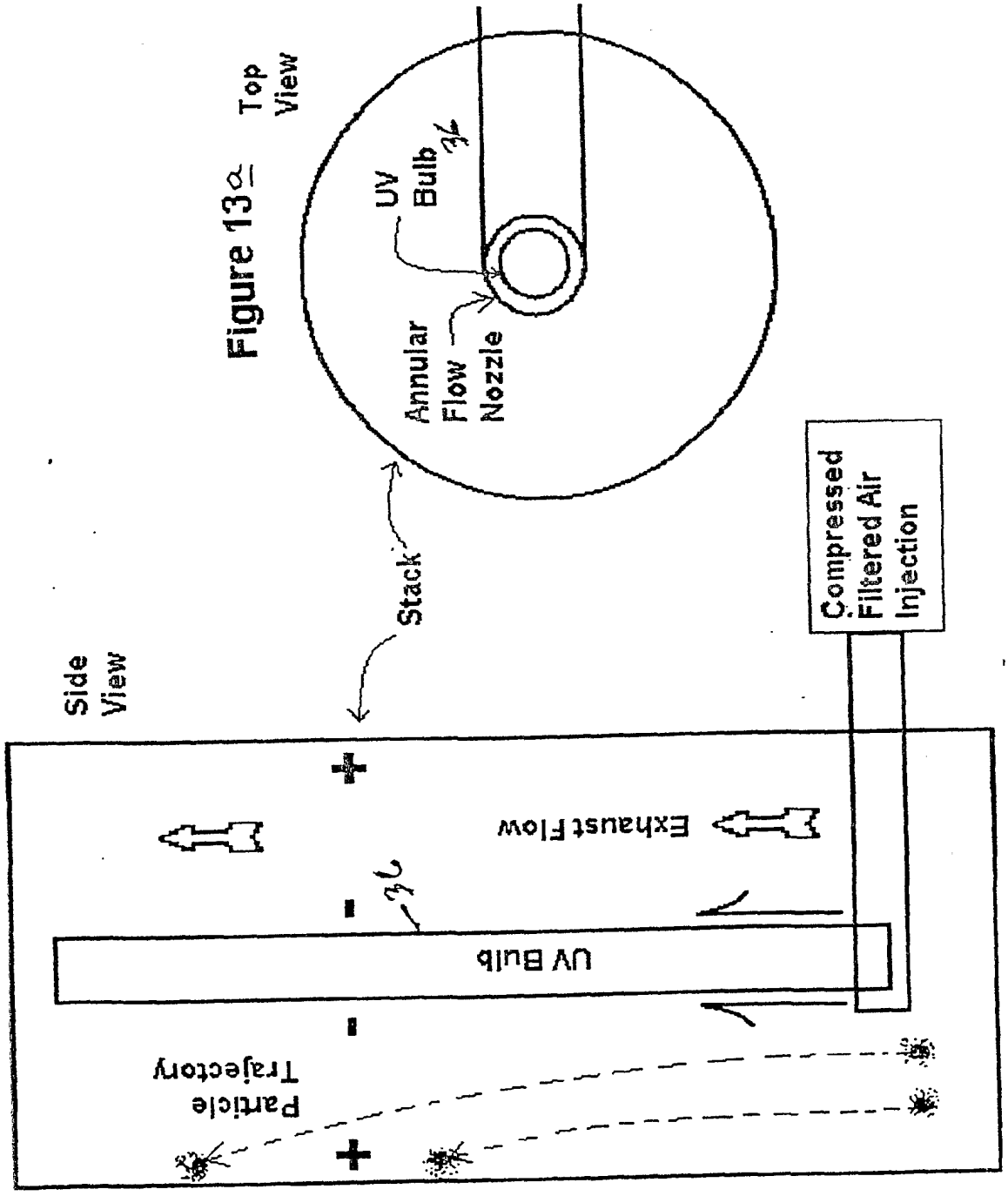


Figure 13 - Electrostatic Field + Boundary Layer of Clean Gas Protection of Ultraviolet Bulb in Very Dirty Exhaust Gases

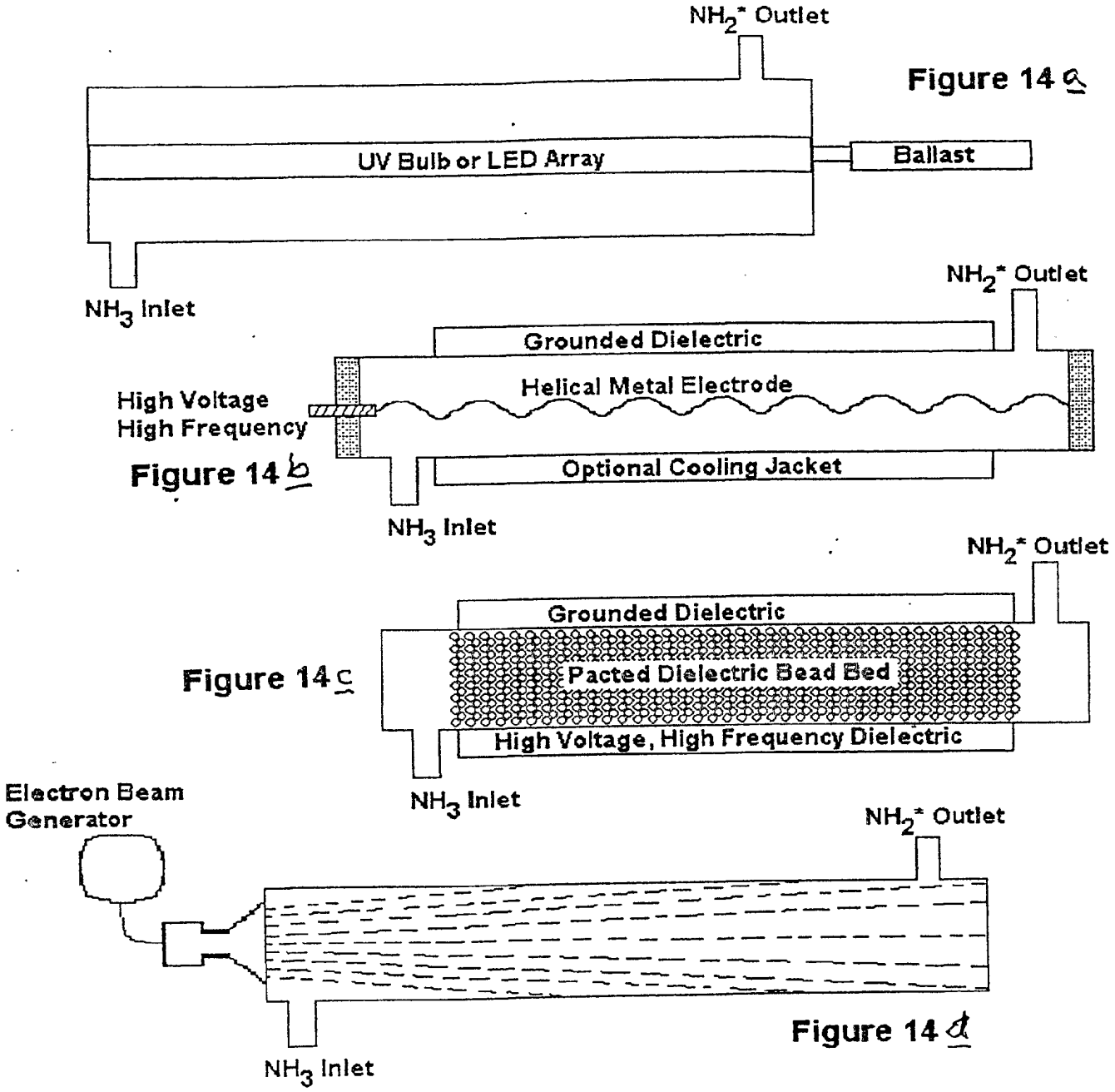


Figure 14 - Amidogen Radical (NH_2^*) Generators

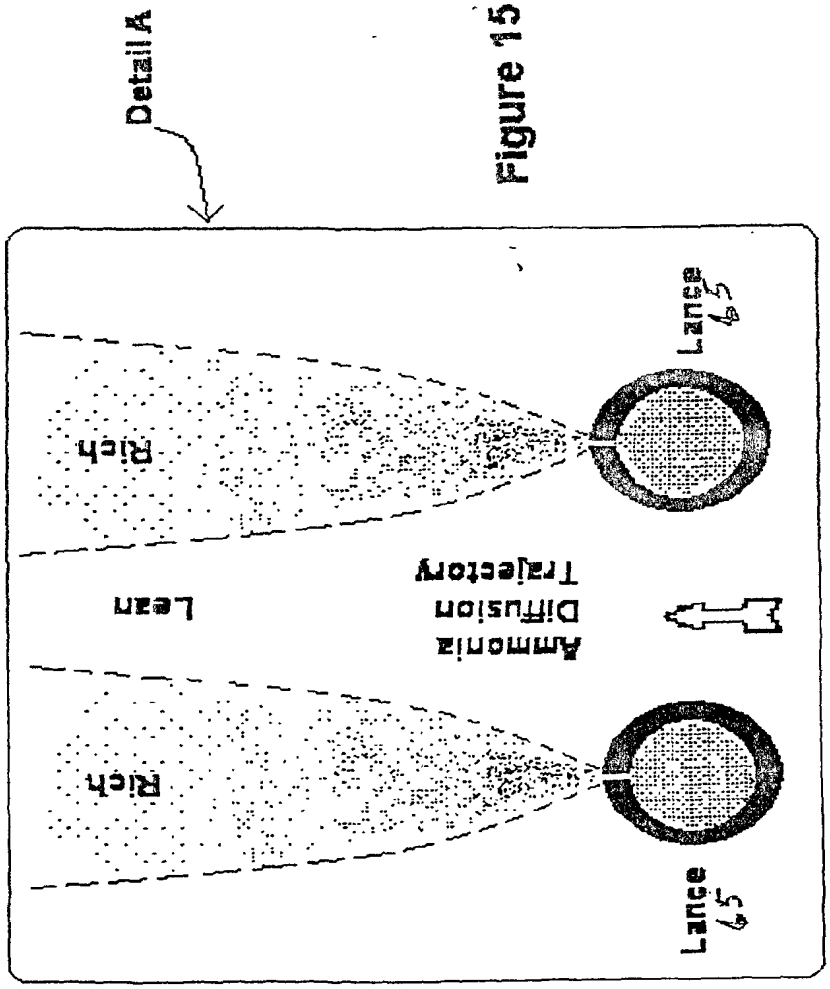


Figure 15a

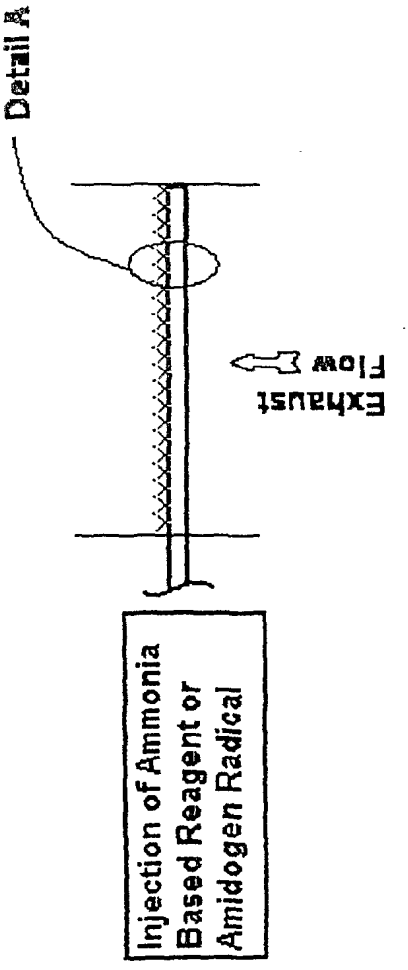


Figure 15 - Demonstration of ammonia gas mixing with lance or wall nozzle injection

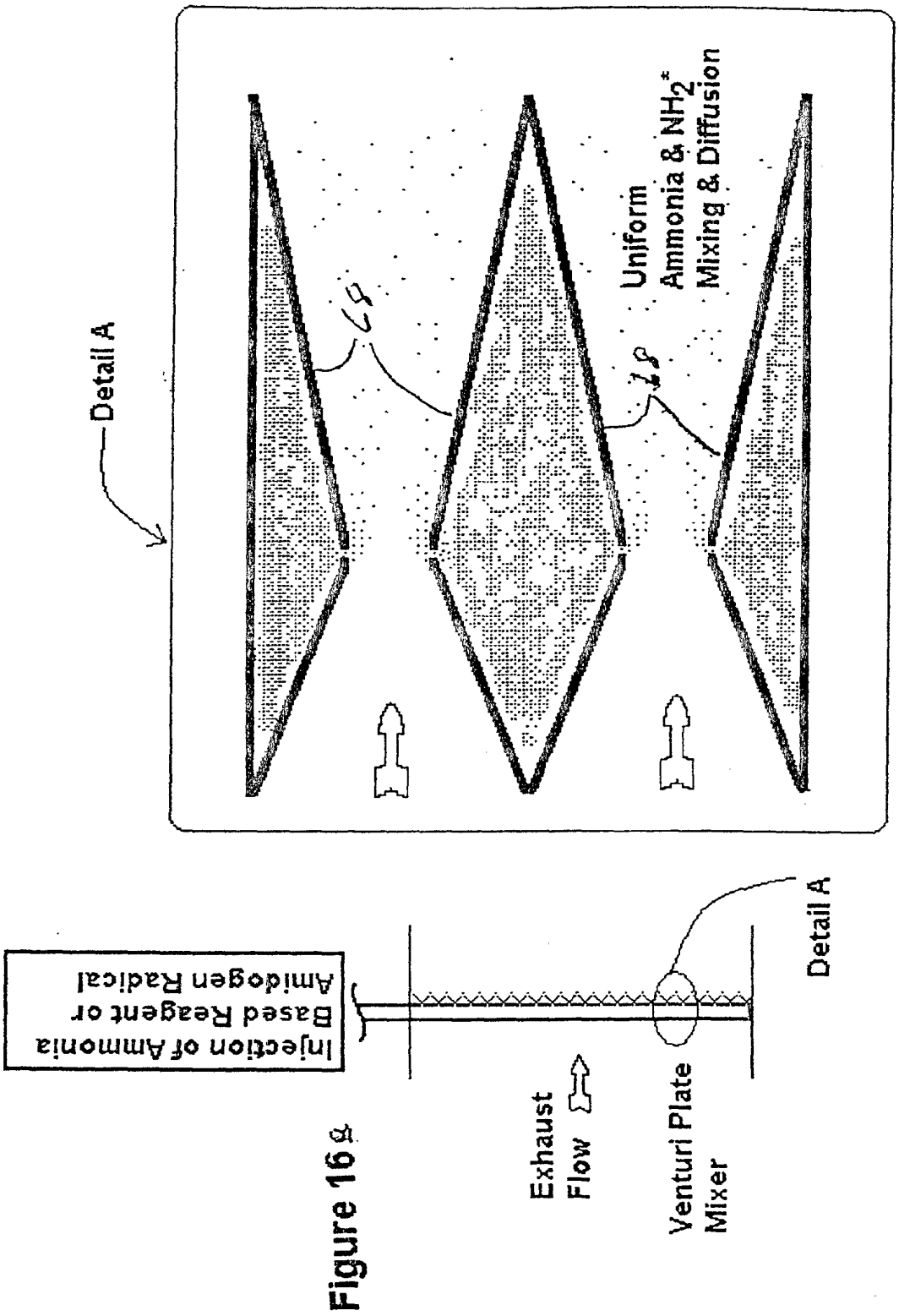


Figure 16a

Figure 16 - Demonstration of ammonia gas mixing with a Venturi Plate

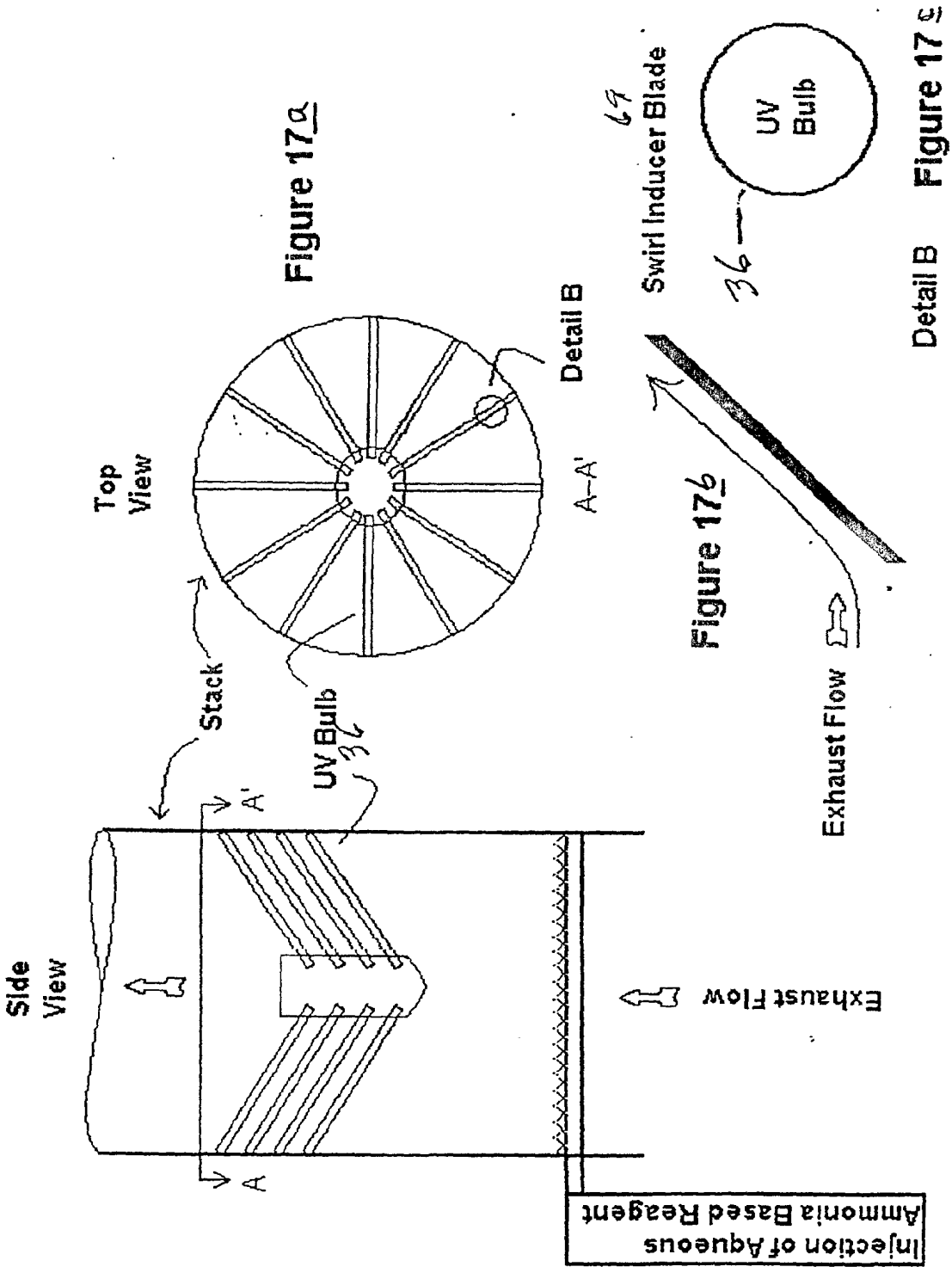
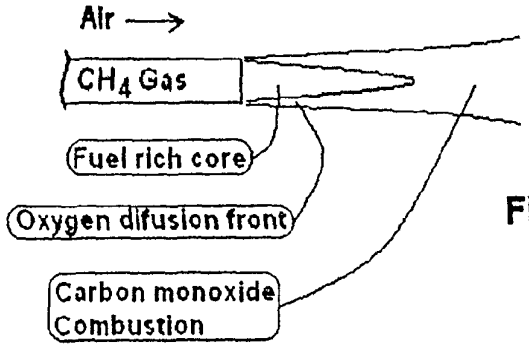
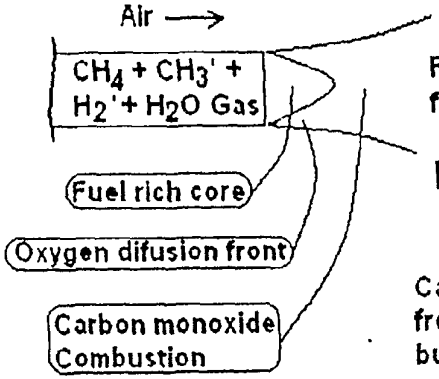


Figure 17 - Installation of the SJVR process on a hot exhaust stack using the vaporization of water to cool the exhaust gases and the thermal decomposition of urea to supply the ammonia



Typical Thermally Ignited Flame Front

Figure 18a



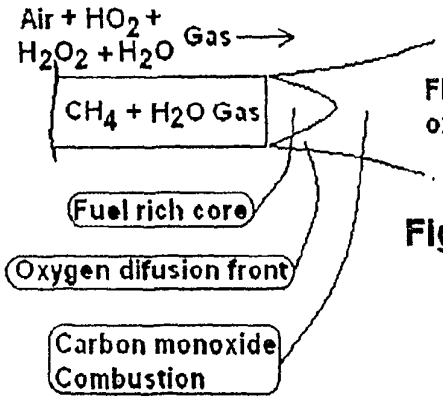
Flame ignited with free fuel based radicals

Figure 18b

Fuel based free radicals generated with the addition of 1-2% air or 1-4% water vapor added to fuel then exposed to ultraviolet light, dielectric barrier discharge, electron beam, or laser discharge.

Liquid Fuel requires longer residence time and higher water vapor content to promote gasification of liquid without coking. Reformer generated hydrogen gas can also be used to dilute liquid fraction.

Care must be taken to generate free radicals close enough to burner tip to prevent significant recombination before flame front



Flame ignited with free oxygen based radicals

Figure 18c

Oxygen based free radicals generated with the addition of 1-3% water vapor added to air then exposed to ultraviolet light, dielectric barrier discharge, electron beam, or laser discharge.

Figure 18 - Use of SUVR at burner to reduce VOC emissions, Increase Flame speed, and reduce NOx emissions

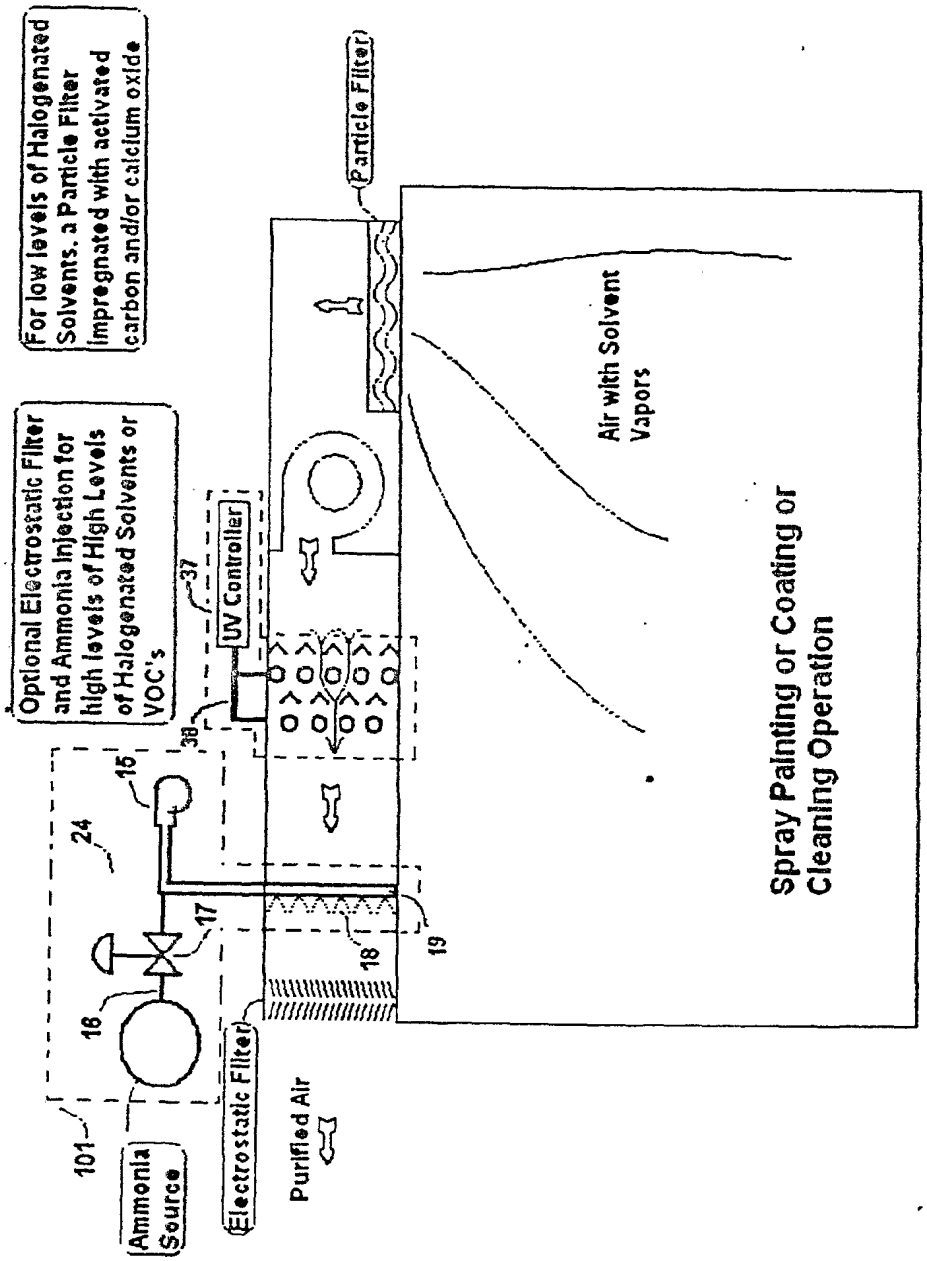


Figure 19 - Organic Compound Destruction Using SUVR with Optional Halogen Acid Removal

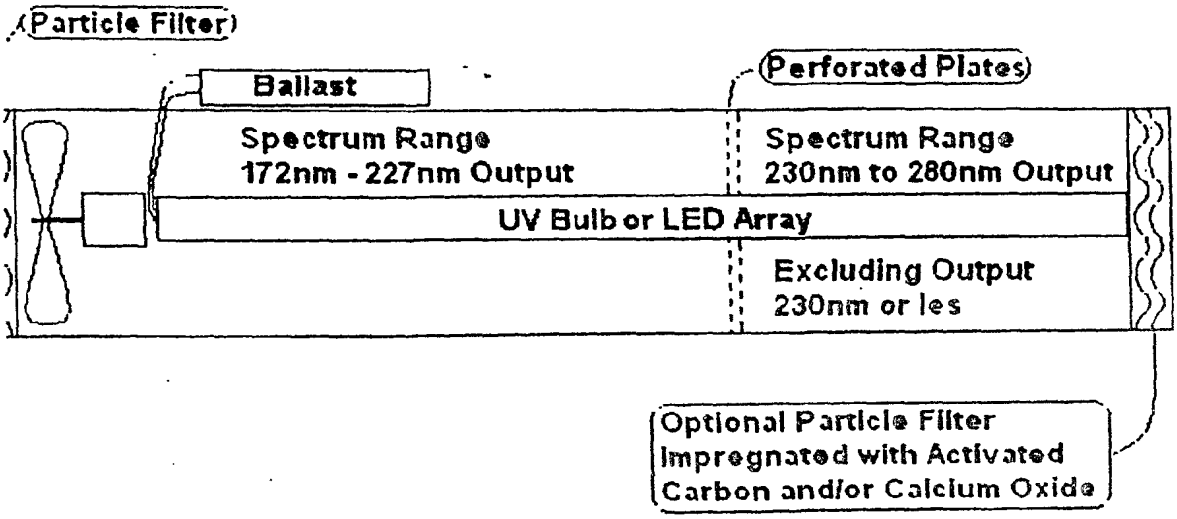


Figure 20 - Portable SUVR unit for Organic Compound Destruction